

Maria D. Plotnikova , Marina G. Shcherban' <sup>\*</sup> , Anastasia D. Shitoeva ,  
Alexander N. Vasyanin , Anatoly B. Shein 

*Perm State University, Perm, Russia*

(\*Corresponding author's e-mail: [ma-she74@mail.ru](mailto:ma-she74@mail.ru))

## The Role of Surface Hydrophobization of Mild Steel by Some Triazole Derivatives in Acidic Medium

Triazole derivatives (4,5-diphenyl-4H-1,2,4-triazole-3-thiol (4,5-PhTAT) and 3,4-diphenyl-5-(prop-2-yn-1-ylthio)-4H-1,2,4-triazole (3,4-PhPTTA) have been researched as corrosion inhibitors for mild steel in 0.1 N sulfuric acid solution. Electrochemical methods were used to estimate the corrosion rate and the inhibition efficiency: potentiodynamic polarization and impedance spectroscopy. The semi-empirical GFN2-xTB method, taking into account their implicit solvation in water using the ALPB method in the XTB program have been used for Geometry optimization of the structures of individual compounds and protomers in solution. Quantum chemical calculations suppose predominantly protonated structure for 3,4-PHPTTA molecules and neutral form of molecules for 4,5-PhTAT. According to electrochemical measurements the best inhibition efficiency for 4,5-PhTAT achieved at 50 mg·l<sup>-1</sup> and 200 mg·l<sup>-1</sup> for 3,4-PhPTTA. 4,5-PhTAT and 3,4-PHPTTA are the mix-type inhibitors in 0.1 N sulfuric acid solution, but rate of cathodic process is decreased more than anodic. Contact angle measurements were carried out by the sessile drop method. Hydrophobization of the steel surface occurs in the blank acid and inhibited solution. The contact angle measurements by two test liquids (water and diethylene glycol) after corrosion with presents 4,5-Pstat and 3,4-PHPTTA show that the protective film formed in inhibited solution.

**Keywords:** corrosion, inhibitor, triazoles, polarization curves, surface tension, impedance spectroscopy, quantum chemical calculations, sessile drop method.

### Introduction

Corrosion is a widely studied field of science. The use of inhibitors to control the corrosion in acid medium was found to have widespread applications [1–4]. The corrosion inhibition of steel in acidic medium by organic inhibitors was studied in considerable detail. Triazoles derivatives are N-heterocyclic compounds containing a five-member ring with three nitrogen atoms. Their molecules play important roles in biology due to their extensive biological interactions [4] and in chemistry due to their ability to inhibit corrosion of metals and alloys [1–3]. Today heterocycles inhibitors leading to minimize the corrosion process in metals [5–7]. The use of heterocycles inhibitors is of significant interest because of their economical synthesis methods and high protection efficiency [8, 9]. Among them, triazole derivatives have been researched as effective corrosion inhibitors for steel in acidic media [6, 7]. The inhibition efficiency depends on many factors: the nature of the metal surface, the inhibitor molecular structure — the number of adsorption active centers in the molecule, the charge density, the molecular size, and the ability of this molecule to interact with a metal surface. In order to understand action mechanisms of corrosion inhibitors, there are numerous experimental (electrochemical) [8, 9] and theoretical (quantum chemical) [10, 11] studies. One of the key approaches is the film theory of inhibitors [12, 13], according to the inhibition efficiency is due to the formation of a hydrophobic film on the metal surface. This film can be investigated by the sessile drop method [12–18]. The energy of the surface changes when the inhibitor film is formed and some adsorption centers appear and disappear on it. This can be measured by the method of steel surface contact angles with tested liquids and calculated the components (polar and dispersion) of the free surface energy with increase in the inhibitor concentration. The purpose of this work is to study the protective effect of some triazole derivatives against corrosion of low-carbon steel and to confirm the film theory of adsorption of organic heterocyclic corrosion inhibitors by both experimental electrochemical, surface physico-chemical methods and theoretical quantum chemical calculations.

### Experimental

The tested inhibitors, namely 4,5-diphenyl-4H-1,2,4-triazole-3-thiol (4,5-PhTAT) and 3,4-diphenyl-5-(prop-2-yn-1-ylthio)-4H-1,2,4-triazole (3,4-PhPTTA), were synthesized according to a previously described experimental procedure [6, 18]. The concentration range of both inhibitors was 10–200 mg·l<sup>-1</sup>.

Geometry optimization of the structures of individual compounds was carried out using the semi-empirical GFN2-xTB method, taking into account their implicit solvation in water using the ALPB method in the XTB program [19, 20]. The calculation of the mole fractions of individual protomers in solution at 298.15 K was performed using the Boltzmann distribution based on the computed Gibbs energies of the optimized structures. The estimation of the protonation constants of compounds was done using the ChemAxon Marvin pK<sub>a</sub> Plugin [21].

Electrochemical measurements were carried out using the electrochemical system Solatron 1280C. Steel potentials were measured relative to a silver chloride electrode. Potentiodynamic polarization and impedance measurements were performed using a glass electrochemical cell with an external space for silver chloride and counter platinum electrodes. Voltammetric studies were performed according to a three-electrode scheme in potentiodynamic mode at a working electrode potential sweep rate of 0.5 mV·s<sup>-1</sup>. Prior to polarization, the electrode was kept in the test solution for 30 min to establish a free corrosion potential, E<sub>cor</sub>. Impedance measurements were recorded in the range of frequencies *f* from 20 kHz to 0.1 Hz, a sine wave with 5 mV amplitude was used to perturb the system. The criterion for estimating equivalent electrical circuits was the  $\chi^2$  parameter calculated in ZView2. A satisfactory equivalent scheme is for  $\chi^2$  less than 10<sup>-3</sup> when weight coefficients calculated from experimental values of the impedance modulus. All potentials are reported vs standard hydrogen electrode.

Working electrodes with the composition, wt.%: Fe — 98.27; C — 0.20; Mn — 0.50; Si — 0.30; P — 0.04; S — 0.04; Cr — 0.15; Ni — 0.30; Cu — 0.20, were used in the study. The experiments were conducted in 0.1 N solution were prepared from chemically pure H<sub>2</sub>SO<sub>4</sub> and distilled water.

The corrosion rate, *ICR* (cm·s<sup>-1</sup>), was estimated through the following equation combining Stern-Geary and Faraday equations:

$$ICR = (MB)/(zFS\rho R_p),$$

where *M* is average molecular weight of the metal or metal alloy (g·mol<sup>-1</sup>), *S* is the surface area (cm<sup>2</sup>), *F* is the Faraday constant [96 485 A·s·mol<sup>-1</sup>], *z* is the average charge of the metal, and  $\rho$  is the density of the metal (g·cm<sup>3</sup>), *B* is the Stern-Geary constant (V) defined as  $B = b_a b_c / 2.3(b_a + b_c)$ , *R<sub>p</sub>* is polarization resistance, ( $\Omega$ ). Units of corrosion rate in this paper are given in mm·year<sup>-1</sup>.

According to the theory of polarization resistance the *R<sub>p</sub>* method is based on charge balance and the current-potential relationship (Tafel relationship) for electron-transfer reactions. *R<sub>p</sub>* is defined as the differential of the overpotential,  $\Delta E$  (volt), over the withdrawn current, *i<sub>corr</sub>* (amp), when the slope of polarization curve at the corrosion potential:

$$R_p = dE/di = b_a b_c / 2.3i_{\text{corr}}(b_a + b_c) = B/i_{\text{corr}},$$

where *b<sub>a</sub>* and *b<sub>c</sub>* are anodic and cathodic Tafel constants (volt), *i<sub>corr</sub>* is the corrosion current (A·cm<sup>-2</sup>) [22, 23].

The inhibition efficiency for each concentration of inhibitors was calculated according to the equation,

$$IE(\%) = (1 - i_{\text{corr}}/i_{0\text{corr}}) \cdot 100,$$

where *IE*, is the inhibition efficiency, *i<sub>corr</sub>* and *i<sub>0corr</sub>* are the corrosion current densities (A·cm<sup>-2</sup>) with and without inhibitor, respectively. The corrosion current density (*i<sub>corr</sub>*) was determined by extrapolating the Tafel lines.

On the basis of Young's equation plus Owen-Wendt's theory, the surface free energies of the steel surface can be calculated using the contact angles between the two test liquids (water and diethylene glycol) and steel surface [25]. Contact angle measurements were carried out using a tensiometer DSA 25E (KRÜSS) by the sessile drop method [26]. Test liquids (liquid with known the value of surface tension) were dropped to the surface of the sample using a dispenser, after that the angle between three phases (steel, test liquid and air) was measured. The volume of test liquids was 1–2  $\mu$ l. All the experiments were carried out after immersion of mild steel for 24 hours in 0.1 N H<sub>2</sub>SO<sub>4</sub> in absence and presence of different concentrations of inhibitors. After immersion samples were cleaned with distilled water repeatedly and dried in hot air, then the contact angles were measured.

## Results and Discussion

Based on the structural characteristics of 4,5-PhTAT, it is reasonable to posit that this compound exhibits amphoteric behavior in aqueous systems, where it can undergo both protonation and deprotonation reactions. According to free energy calculations, the tautomeric form with proton moved to the N atom dominates in the neutral state (Figure 1).

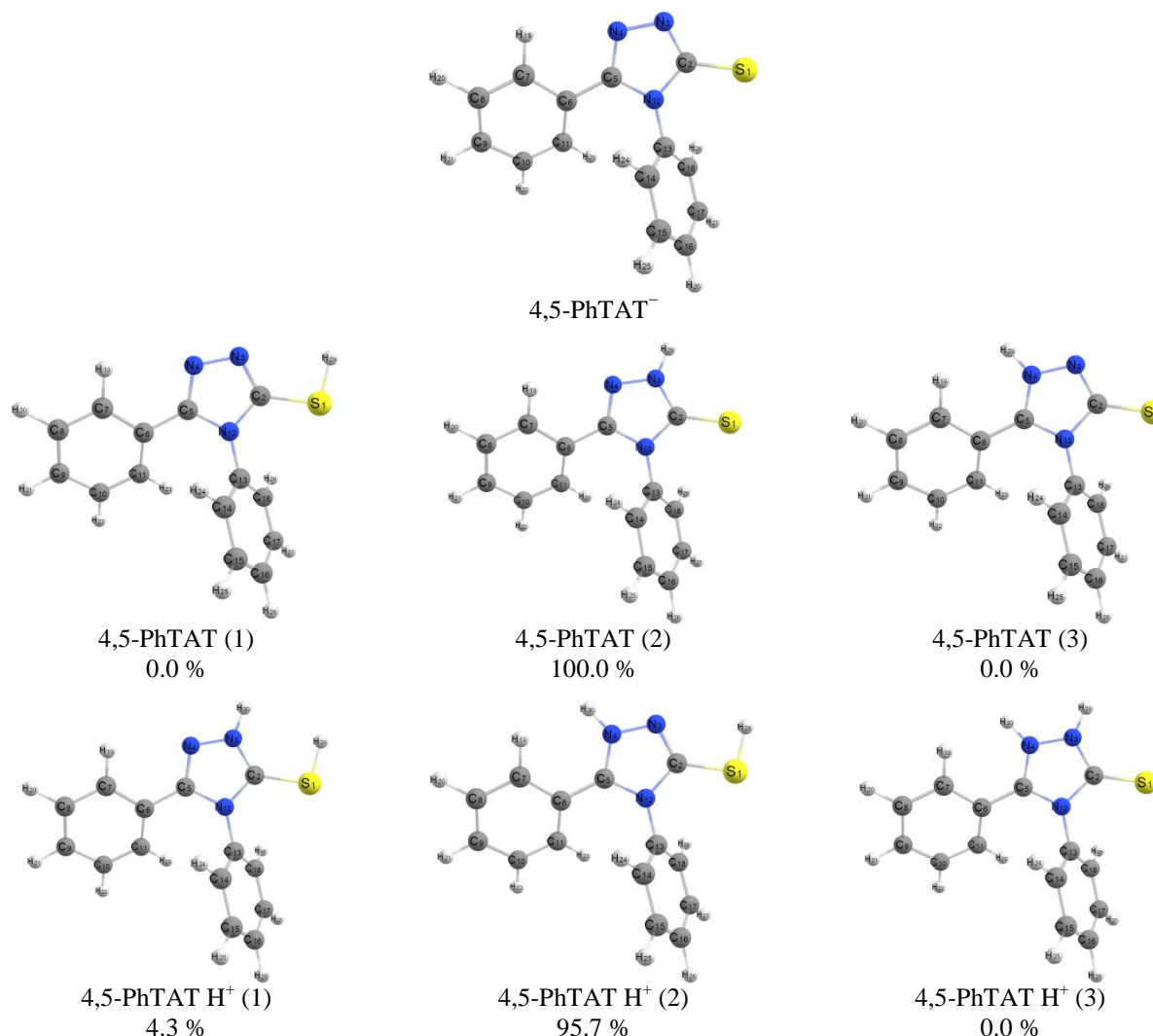


Figure 1. The optimized geometries of the deprotonated molecule (anion) 4,5-PhTAT, as well as the tautomers of the neutral molecule and its mono-protonated form obtained at the GFN2-xTB[ALPB(H<sub>2</sub>O)] theory level with their relative fractions (%) in solution at 298.15 K

The protonation/deprotonation equilibrium constants were computed using the Marvin  $pK_a$  Plugin program, taking into account tautomerization. The results indicate that deprotonation is the only feasible outcome in solutions with weakly alkaline properties ( $pK_a = 7.21$ ). Conversely, the calculations strongly suggest that protonation is practically unattainable, as evidenced by the extremely low predicted value of the corresponding equilibrium constant ( $pK_a = -4.65$ ). Notably, the calculations reveal that among the three feasible tautomers of the protonated form present in solution, the 4,5-PhTAT H<sup>+</sup> (2) tautomer is expected to be the predominant species.

#### Protonation of 3,4-PHPTTA

Only protonation processes are possible for 3,4-PHPTTA. In contrast to 4,5-PhTAT, protonation of 3,4-PHPTTA is entirely possible in strongly acidic aqueous solutions (with a  $pK_a$  value of 0.97 for the 3,4-PHPTTA H<sup>+</sup> (1) form and 0.22 for the 3,4-PHPTTA H<sup>+</sup> (2) form). The calculation of the molar fraction of monoprotonated forms using the GFN2-xTB[ALPB(H<sub>2</sub>O)] method agrees well with the results obtained from the Marvin  $pK_a$  Plugin and confirms the predominance of the 3,4-PHPTTA H<sup>+</sup> (1) protomer (Figure 2).

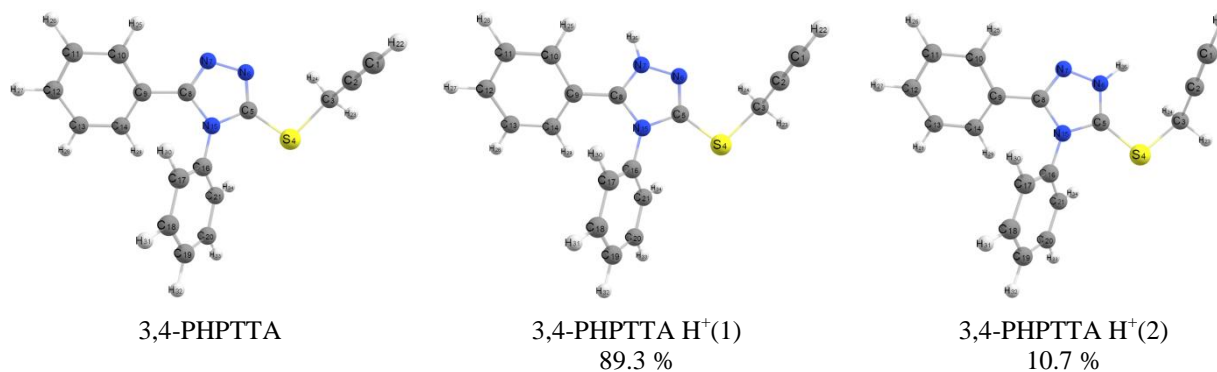


Figure 2. The optimized geometries of the neutral molecule 3,4-PHPTTA and its monoprotonated tautomers obtained at the GFN2-xTB[ALPB(H<sub>2</sub>O)] level of theory with their relative fractions (%) in solution at 298.15 K

Based on the results of the calculations, it was shown that in acidic H<sub>2</sub>SO<sub>4</sub> solutions, inhibitors 4,5-PhTAT and 3,4-PHPTTA exist in different forms: 3,4-PHPTTA molecules are predominantly protonated, while 4,5-PhTAT exists as neutral molecules.

Polarization curves for mild steel in 0.1 N H<sub>2</sub>SO<sub>4</sub> solution without and with addition of 100 mg·l<sup>-1</sup> of 4,5-PhTAT and 3,4-PhPTTA are shown in Fig. 3.

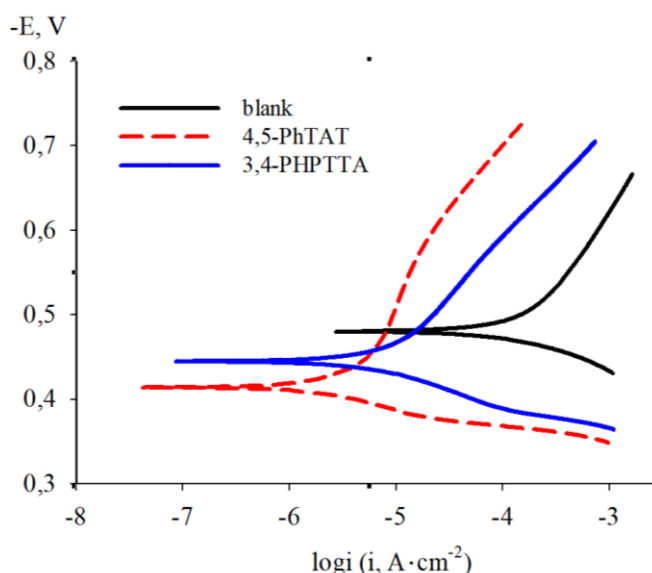


Figure 3. Potentiodynamic polarization curves for mild steel in 0.1 N H<sub>2</sub>SO<sub>4</sub> with different triazole derivatives

Analysis of Figure 3 and Table 1 reveals that the presence of both triazoles resulted in a shift of the corrosion potential towards the anodic direction in comparison with the result obtained in the blank acid solution (Table 1). The anodic and the cathodic current densities were decreased, indicating that 4,5-PhTAT and 3,4-PhPTTA suppressed both the anodic and cathodic reactions (Figure 3).

Table 1 shows that in the case of 4,5-PhTAT corrosion current decreased already at 10 mg·l<sup>-1</sup> and had minimal value at 50 mg·l<sup>-1</sup>, then it slightly increased with the growth concentration. If added to the system 3,4-PhPTTA, corrosion currents slowly decrease with increasing concentration, it appears from 50 mg·l<sup>-1</sup>.

Figure 3 demonstrates that polarization curves show two linear parts in the anodic region in the presence of inhibitors, but Table 1 shows only Tafel coefficients near by corrosion potential. It is shown that, the injection of inhibitors decreased the rate of cathode process greater than anodic, as the  $b_c$  has increased with raising concentration. According to linear polarization results, the corrosion rate decreases from 1.13 mm·year<sup>-1</sup> to 0.023 and 0.049 mm·year<sup>-1</sup> (47 and 23 times) with presence 4,5-PhTAT and 3,4-PhPTTA respectively.

**Polarization Parameters for Mild Steel in 0.1 N H<sub>2</sub>SO<sub>4</sub> Solution Containing Different Concentrations of 4,5-PhTAT and 3,4-PhPTTA at 298 K**

Inhibitor	C, mg·l <sup>-1</sup>	Tafel polarization				Linear polarization	
		$-E_{\text{corr}}$ , mV	$i_{\text{corr}}$ , A·cm <sup>-2</sup>	$b_a$ , mV	$b_c$ , mV	$R_p$ , Ω	ICR, mm·year <sup>-1</sup>
–	–	677	$8.34 \cdot 10^{-5}$	51	125	190	1.13
4,5-PhTAT	10	625	$3.56 \cdot 10^{-5}$	53	132	2994	0.041
	50	619	$2.45 \cdot 10^{-6}$	55	140	5154	0.023
	100	614	$2.09 \cdot 10^{-6}$	54	160	4831	0.024
	200	604	$2.87 \cdot 10^{-6}$	51	189	4466	0.033
3,4-PhPTTA	10	672	$8.10 \cdot 10^{-5}$	48	120	200	1.25
	50	654	$9.19 \cdot 10^{-6}$	45	130	1603	0.11
	100	645	$7.15 \cdot 10^{-6}$	47	158	1943	0.083
	200	601	$4.18 \cdot 10^{-6}$	50	157	2493	0.049

Figure 4 shows the Nyquist diagrams of impedance data of mild steel in 0.1 N sulfuric acid solution with different concentrations 4,5-PhTAT and 3,4-PhPTTA. Impedance spectra in pure acid solution is presented as the insertion on one of the diagrams. These diagrams (Figure 4) at  $E_{\text{corr}}$  are characterized by a depressed capacitive semicircle at high to medium frequencies. The dispersion is explained by surface heterogeneity due to surface roughness [26, 27]. Hence the inhibition efficiency has a tendency to grow as the values of  $R_{\text{ct}}$  increase.

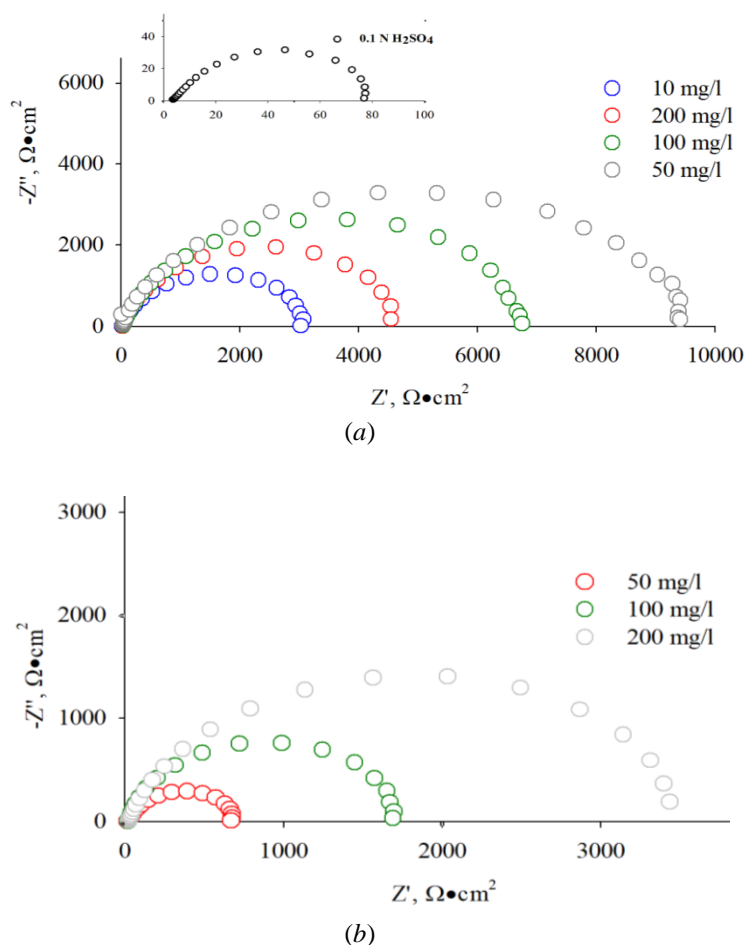


Figure 4. Nyquist diagrams of mild steel in a solution of 0.1 N H<sub>2</sub>SO<sub>4</sub> at  $E_{\text{corr}}$  with addition of various concentration of (a) and (b) 3,4-PhPTTA

The calculation results correlate with the electrochemical results. 4,5-PhTAT gives a greater inhibition efficiency than 3,4-PhPTTA at low concentration due to the neutral form of molecules. The protonated form of 3,4-PhPTTA molecules at low concentration are pushed off the surface of mild steel with positive charge in sulfuric acid solution.

The calculation of the free surface energy (SFE) of steel was carried out before and after contact with a corrosive medium to confirm the assumptions about the formation of the protective film and the chemical nature of adsorption. The value of SFE due to the isolation of its polar ( $\gamma^p$ ) and dispersion ( $\gamma^d$ ) components can indicate the direction of further modification to increase resistance of the corrosion system.

The surface energy parameters were calculated based on the analysis of the Owen-Wendt's equation:

$$W_a = \gamma_{LG}(1 + \cos\theta_c) = 2(\gamma_{SG}^d \gamma_{LG}^d)^{0.5} + 2(\gamma_{SG}^p \gamma_{LG}^p)^{0.5},$$

where  $W_a$  — work of adhesion,  $\gamma_{LG}$  — the liquid/air interfacial tension,  $\gamma_{SG}^d$ ,  $\gamma_{SG}^p$  — polar and dispersive component of surface energies of steel,  $\gamma_{LG}^d$ ,  $\gamma_{LG}^p$  — polar and dispersive component of surface tension of test liquids,  $\cos\theta_c$  — the contact angle for test liquids at steel surface after corrosion.

Fig. 5 demonstrates images of test liquids drops on the steel surface after exposition in corrosion medium with inhibitors during 24 hours.

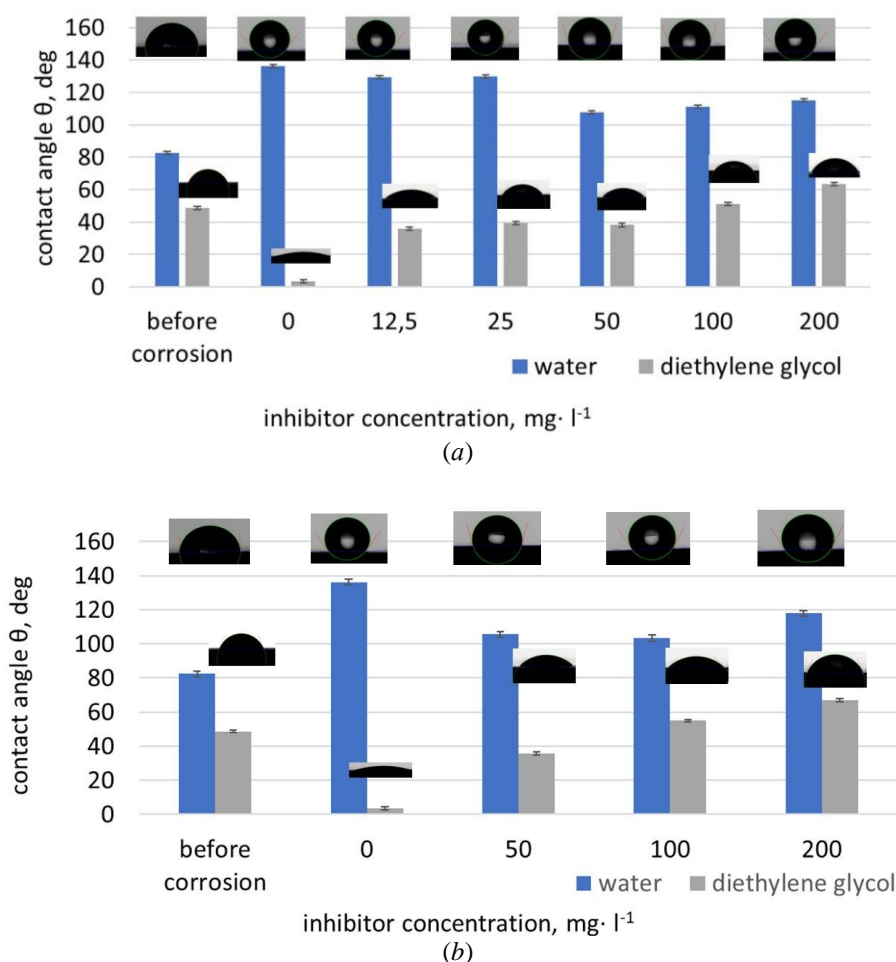


Figure 5. Surface wettability of steel surface after corrosion in 0.1 N H<sub>2</sub>SO<sub>4</sub> solution with (a) 4,5-PhTAT and (b) 3,4-PhPTTA

In general, the steel surface before corrosion has a hydrophilic character, since metals and metal alloys have high surface energy values and wettability by liquids with lower surface tensions. Thus, the surface energies of ferrite and cementite are 2482 and 2050 mJ·m<sup>-2</sup> [25], these steel phases are wetted by water with surface tension 72 mJ·m<sup>-2</sup> [28]. According to [29], the contact angle of mild steels by water is about 64° [30]. In our case, the contact angle is 82°, this value is close to the contact angle on pyrolytic graphite (83.9°). This allows to propose that the surface is enriched by carbon.

The contact angle increased to  $136^\circ$  after exposure of samples in pure sulfuric acid that leads to surface hydrophobization significantly. After that surface roughness increased as a result of iron dissolution and surface enrichment by carbon — the contact angles are close to those of fine-dispersed graphite and graphene [28, 29]. The hydrophobicity is also shown by the wettability of the steel by less polar liquid after immersion in pure acid. The contact angles decrease from  $48^\circ$  to  $3^\circ$ , if the test liquid is changed from water to diethylene glycol.

The steel surface is also hydrophobized in the presence of the inhibitors (contact angles range from  $105^\circ$  to  $130^\circ$ ); however, this is caused by other reasons. In this case, the hydrophobicity increased probably due to the formation of a protective film of inhibitor on the steel surface. The contact angle of the primary steel surface is  $48,7^\circ \pm 0,9^\circ$ , then after corrosion in sulfuric acid it is decreased to  $3,6^\circ \pm 0,5^\circ$  and finally the contact angle in presence of inhibitors changes in the range of  $35\text{--}70^\circ$ . There is a tendency to growth with increasing inhibitor concentration.

These changes in the wettability of test liquids after corrosion indicate a different state of steel surface. Figure 6 demonstrates the redistribution of the polar and dispersion components of the free surface energy, its values and the inhibition efficiency are given in Table 2.

The immersion of the samples in blank sulfuric acid leads to significant hydrophobization of the steel surface, the contact angle increases to  $136^\circ$  as a result of the dissolution of iron and the surface enrichment with carbon [32, 33].

The steel surface in the presence of an inhibitor is also hydrophobized — the contact angles are in the range of  $105^\circ\text{--}130^\circ$ . Probably, the effect of hydrophobization of the surface is associated with the formation of a protective film of the inhibitor, and not with the increase of the carbon concentration on the steel surface.

Also the ratio of the polar and dispersion components of the free surface energy changes when samples are kept in inhibited acid. Calculated SFE values and the degrees of protection calculated from the results of weight loss testing are presented in Table 2.

Table 2.

Surface energies for test liquids ( $22^\circ\text{C}$ ) and degree of protection of St3 after weight loss tests in the presence of triazole derivatives in  $0.1\text{ N H}_2\text{SO}_4$  solution

Conc., $\text{mg}\cdot\text{l}^{-1}$	$\gamma_{\text{SG}}^{\text{p}}, \text{mJ}\cdot\text{m}^{-2}$	$\gamma_{\text{SG}}^{\text{d}}, \text{mJ}\cdot\text{m}^{-2}$	$\gamma_{\text{SG}}, \text{mJ}\cdot\text{m}^{-2}$	$\gamma_{\text{SG}}^{\text{d}}/\gamma_{\text{SG}}^{\text{p}}$	Z, %
Before immersion	6,2	24,98	31,18	4,0	
0	43,4	149,96	193,32	3,5	
4,5-PhTAT					
50	3,73	70,19	73,92	18,8	96
100	6,40	78,18	84,58	12,2	92
200	9,25	83,96	93,21	9,1	92
3,4-PhPTTA					
50	1,13	53,40	54,53	47,3	94
100	1,06	42,12	43,18	39,7	95
200	2,53	43,28	45,82	17,3	95

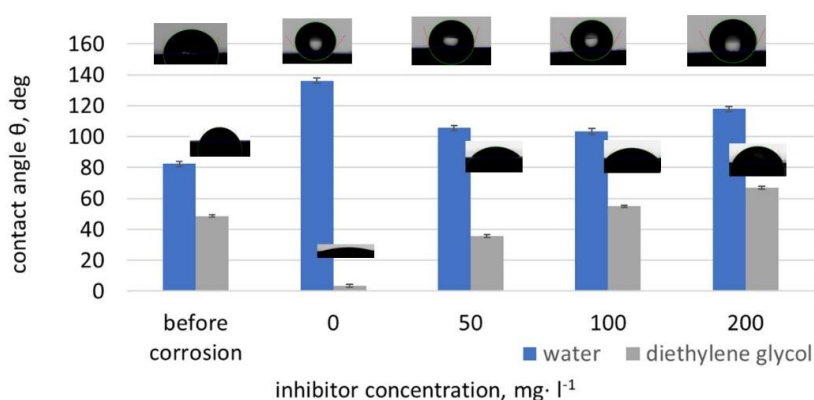


Figure 6. The effect of redistribution of the free surface energy with increasing concentration of inhibitors

4,5-PhTAT has higher value of ratio dispersion and polar components of the free surface energy (Table 2). 4,5-PhTAT forms hydrophobic film at low concentration and due to has inhibition properties already at  $10 \text{ mg}\cdot\text{l}^{-1}$ . 3,4-PhPTTA doesn't have inhibition activity at low concentration.

### Conclusions

1. 4,5-diphenyl-4H-1,2,4-triazole-3-thiol (4,5-PhTAT) and 3,4-diphenyl-5-(prop-2-yn-1-ylthio)-4H-1,2,4-triazole (3,4-PhPTTA) act as good inhibitors for mild steel in 0.1 N  $\text{H}_2\text{SO}_4$ , the rate of corrosion is reduced by 47 and 23 times, respectively. The inhibition efficiency depended from concentration: 4,5-PhTAT has the best inhibition efficiency value at  $50 \text{ mg}\cdot\text{l}^{-1}$  and 3,4-PhPTTA only at  $200 \text{ mg}\cdot\text{l}^{-1}$ .

2. Polarization curves proved that 4,5-PhTAT and 3,4-PhPTTA were mixed type inhibitors, but which can suppress cathodic reactions more. Impedance plots indicated that  $R_{ct}$  values increase as well as shown in polarization results. Theoretical calculations provide good support to experimental electrochemical results.

3. The steel surface in the presence of both compounds becomes more hydrophobic, as the contact angle increases from  $82^\circ$  to  $120^\circ - 130^\circ$  depending on the inhibitor concentration. Also, the free surface energy of steel decreases in the presence of inhibitors compared to pure acid (from  $193 \text{ mJ}\cdot\text{m}^{-2}$  to  $46 - 74 \text{ mJ}\cdot\text{m}^{-2}$ ), and the SFE components are redistributed: the contribution of the dispersion component with adding triazole derivatives in corrosion media to the total value of SFE increases by 3-4 times compared to the test steel surface.

4. Redistribution in polar and dispersion components consist of different forms of molecular existence: 3,4-PhPTTA is predominantly protonated, while 4,5-PhTAT is neutral molecules according to quantum chemical calculation.

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Information about authors\*

**Plotnikova, Maria Dmitrievna** — Candidate of Chemical Sciences, Assistant Professor of Physical Chemistry Department, Perm State National Research University, Bukireva st., 15, 614990, Perm, Russia; e-mail: [plotnikova-md@mail.ru](mailto:plotnikova-md@mail.ru); <https://orcid.org/0000-0002-4050-5682>

**Shcherban', Marina Grigoryevna** (*corresponding author*) — Candidate of chemical sciences, Assistant professor of Physical Chemistry Department, Perm State National Research University, Bukireva st., 15, 614990, Perm, Russia; e-mail: [ma-she74@mail.ru](mailto:ma-she74@mail.ru); <https://orcid.org/0000-0002-6905-6622>

**Shitoeva, Anastasia Dmitrievna** — First-Year Master Student, Perm State National Research University, Bukireva st., 15, 614990, Perm, Russia; e-mail: [shitoeva0910@gmail.com](mailto:shitoeva0910@gmail.com); <https://orcid.org/0009-0005-9611-7848>

**Vasyanin, Alexander Nikolaevich** — Candidate of chemical sciences, Assistant professor of Physical Chemistry Department, Perm State National Research University, Bukireva st., 15, 614990, Perm, Russia; e-mail: [avasyanin@psu.ru](mailto:avasyanin@psu.ru); <https://orcid.org/0000-0002-1991-094X>

**Shein, Anatoly Borisovich** — Doctor of Chemical Sciences, Professor of Physical Chemistry Department, Perm State National Research University, Bukireva st., 15, 614990, Perm, Russia; e-mail: [ashein@psu.ru](mailto:ashein@psu.ru); <https://orcid.org/0000-0002-2102-0436>

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\*The author's name is presented in the order: *Last Name, First and Middle Names*